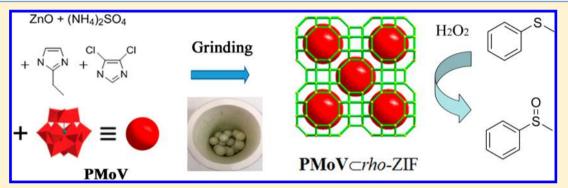




# Efficient Mechanochemical Synthesis of Polyoxometalate⊂ZIF Complexes as Reusable Catalysts for Highly Selective Oxidation

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Supporting Information



ABSTRACT: One-pot mechanochemical synthesis was demonstrated to be an efficient strategy to synthesize host-guest POM⊂rho-ZIF complexes (POM = polyoxometalate; rho-ZIF = zeolitic imidazolate framework with rho topology) with high crystallinity. In this work, the metastable rho-ZIF with large interior cavities and windows was used as host matrix for encapsulating and immobilizing bulky guest molecules with high loading efficiency and chemical stability. As novel catalysts, POMcrho-ZIF complexes were found effective for the selective oxidation of a series of sulfides to sulfoxides. Moreover, the heterogeneity of these composite catalysts was confirmed by leaching tests, and they can be recycled at least four times without significant loss of activity.

## INTRODUCTION

The development of selective and recyclable heterogeneous catalysts is highly desirable yet remains an important challenge. Polyoxometalates (POMs) that possess unique metal-oxygen framework and excellent acid/oxidation catalytic properties have great application prospects in industry. 1,2 Nevertheless, the application of pure POMs is limited by low surface areas as solid catalysts<sup>3</sup> and poor reusability as homogeneous catalysts. To overcome these drawbacks, POMs have been dispersed and immobilized to various supports with high surface areas such as zeolites, silica, activated carbon, mesoporous molecular sieves,<sup>7</sup> and even metal-organic macrocycles.<sup>8</sup> Recently, one of the most attractive strategies for heterogenizing POMs is using metal-organic frameworks (MOFs) as host matrice. 9,10 For instance, Liu<sup>10</sup> and Hill<sup>11</sup> et al. have reported a series of highly crystalline Cu-BTC MOFs (BTC = 1,3,5-benzenetricarboxylic acid) incorporating the protonated POMs in hydrothermal synthesis and used them as effective solid catalysts for the hydrolysis and oxidation reactions. However, the solvothermal synthesis to encapsulate POMs into the cages of an MOF in a "ship-in-a-bottle" manner usually suffered from high temperature, long reaction time, a large excess of active POMs centers, bulky organic solvents, and low loading efficiency. In addition, the relatively closed structure and

confined opening of Cu-BTC MOFs hindered the diffusion of bulky substrates to the active sites, limiting the scope of substrate molecules.

Mechanochemical synthesis 12 is emerging as an alternative method for energy-efficiently constructing MOFs, and it avoids bulk solvents, excess reagents, and harsh conditions. Recently, Friščić et al. presented improved approaches including liquidassisted grinding (LAG) and ion- and liquid-assisted grinding (ILAG) to successfully prepare a number of MOFs. 13,14 Among these MOFs, zeolitic imidazolate frameworks (ZIFs) are extremely attractive host matrice for synthesizing guest⊂MOF materials because of the large interior cages and relatively small windows, which are beneficial for encapsulating and immobilizing bulky guest molecules such as POMs. In 2014, Wang et al. has reported that the hydrophilic unsubstituted Keggin-type POMs can be accommodated into the hydrophobic cavities of the in situ formed ZIF-8 with sod topology in a mechanochemical process.<sup>15</sup> However, catalysis property of this POMCZIF material has not been studied, which is probably due to relatively small windows (3.2 Å) and low POM loading (maximal occupancy is ca. 11% of POM in each cavity).

Received: August 26, 2017 Published: November 16, 2017

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Scheme 1<sup>a</sup>

a) 
$$_{POM + ZnO + (NH_4)_2SO_4}$$
 Grinding  $_{+ HN N}$   $_{+ HN N}$   $_{- HN N}$ 

<sup>a</sup>(a) The process of mechanochemical synthesis of PMoV⊂*rho*-ZIF; the SEM image of PMoV⊂*rho*-ZIF. (b) The structural representation of PMoV⊂ *rho*-ZIF.

Compared with *sod*-type ZIFs, ZIFs with *rho* topology have larger cavities (18.1 vs 12.5 Å) and windows (7.6 vs 3.2 Å), <sup>16</sup> which can greatly favor the porosity accessibility by bulky substrate molecules and accelerate their diffusion rate. In addition, large interior cavities of *rho*-type ZIFs can increase the POM loading ratio and thus enhance the density of active centers. Consequently, exploiting *rho*-type ZIFs as host matrice for encapsulating POMs to prepare POMC*rho*-ZIF materials as heterogeneous catalysts by the one-pot mechanochemical method is very attractive, not only owing to efficient and environmentally friendly synthesis but also because of the abundant porosity and high chemical stability of the host—guest hybrid materials.

In this work, by one-pot mechanochemical synthesis, metastable *rho-*ZIF was used as host matrix for the first time to efficiently synthesize host—guest complexes **PMoV**⊂*rho-*ZIF (**PMoV** = H<sub>4</sub>PMo<sub>11</sub>VO<sub>40</sub>, 1; H<sub>5</sub>PMo<sub>10</sub>V<sub>2</sub>O<sub>40</sub>, 2; H<sub>6</sub>PMo<sub>9</sub>V<sub>3</sub>O<sub>40</sub>, 3) with high crystallinity and chemical stability. In these complexes, POMs were demonstrated to be immobilized within interior cavities of ZIFs with high loading efficiency by physical imprisonment and cannot be released without destroying the host matrice. As novel catalysts, **PMoV**⊂*rho-*ZIFs 1−3 were found effective for selective oxidation of a series of sulfides to sulfoxides or sulfones, including bulky diphenyl sulfides. Additionally, the heterogeneity of these composite catalysts was further verified by leaching tests, and they can be recycled at least four times with no significant loss of activity.

# ■ RESULTS AND DISCUSSION

**Preparation of PMoV** $\subset$ *rho-ZIF.* Because PMoV belongs to the substituted Keggin-type polyoxometalate, the diameter of PMoV is ~10 Å according to the literature, <sup>15a</sup> which can be readily accommodated in the cavities of *rho-ZIF* (18.1 Å). <sup>16</sup> As shown by Scheme 1, PMoV $\subset$ *rho-ZIF* complexes were synthesized by an improved ILAG method, which needs only small amounts of salts and liquid to obviously accelerate the formation of MOFs. After a series of comparative experiments, the optimized amounts of 1 mmol of ZnO, 1.5 mmol of 2-ethylimidazole, 1.5 mmol of 4,5-dichloroimidazole, 10 mg of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, 200  $\mu$ L of *N,N*-diethylformamide, and 0.05 mmol of corresponding PMoV were put into the zirconia milling pot and then ball-milled using zirconia balls for 2 × 30 min.

Notably, the formation of *rho-ZIF* is subtle, and overlong grinding time will lead to appearance of impurity with other topologies. After it was washed with a large mounts of deionized water and alcohol, the green solids were dried under vacuum and collected to afford complexes 1–3. The PMoV/Zn ratios can be adjusted by altering the initial relative amount of PMoV and ZnO. Nevertheless, the targeted products will not form if the ratio exceeds 1:10. In all cases, almost quantitative samples of 1–3 were obtained.

Characterization of PMoV⊂rho-ZIF. Powder X-ray diffraction (XRD) patterns of complexes 1−3 have typical diffraction peaks that match well with the simulated *rho-ZIF* from the single-crystal XRD data, as shown in Figure 1. It is

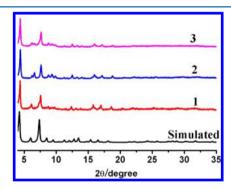


Figure 1. Powder XRD of the simulated rho-ZIF, 1, 2, and 3.

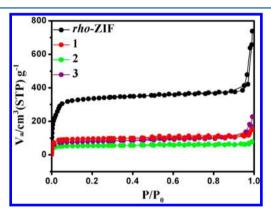
noteworthy that the powder XRD patterns of 1−3 are superior to the original ones of *rho*-ZIF reported by Friščić et al. <sup>12</sup> and close to the samples through solution synthesis by Chen et al. <sup>16a</sup> No diffraction peaks of **PMoV** were observed in these complexes, which indicated that aggregated **PMoV** particles were not formed during the mechanochemical synthesis. Therefore, the original ordered structure of *rho*-type ZIF remained intact after encapsulation of **PMoV**. When the dried samples 1−3 were immersed in various solvents such as water, methanol, ethanol, acetonitrile, and chloroform for 12 h, UV− vis spectra suggested that there were no **PMoV** leaching out from 1−3 and that all of the complexes kept stable crystallinity in these solvents (Figure S1). Compared with the impurity and easy structural transform of pristine *rho*-ZIF by ILAG method, <sup>12b</sup> the high chemical stability of **PMoV**⊂*rho*-ZIF

materials is probably due to strong POM-ZIF interaction from the complementary shape. Besides, the microscopic architecture morphology and granularity of 1 were studied by scanning electron microscopy (SEM) images, which demonstrated that all composites are exactly nanoparticles from 50 to 400 nm (Figure S2).

The Fourier transform infrared (FT-IR) spectra of 1-3 exhibited that the typical characteristic peaks of **PMoV** (1060, 960, 871, and 784 cm<sup>-1</sup>, respectively, corresponding to the P- $O_a$ , Mo =  $O_d$ , Mo- $O_b$ -Mo, and Mo- $O_c$ -Mo band vibrations<sup>18</sup>) and *rho-*ZIF (2971, 1631, 1452, and 1279 cm<sup>-1</sup>) all existed in **PMoV** $\subset$ *rho-*ZIF and proved successful hybridization of **PMoV** and *rho-*ZIF (Figure S3–S5).

Furthermore, the components of **PMoV** $\subset$ *rho-*ZIF were confirmed by inductively coupled plasma atomic emission spectrometry (ICP-AES). Taking 1 as an example, according to the molar ratio of Zn/Mo = 2.75, it represented that ~79.4% cavities of *rho-*ZIFs are occupied by H<sub>4</sub>PMo<sub>11</sub>VO<sub>40</sub>. The ICP-AES results of 2 (Zn/Mo = 2.67) and 3 (Zn/Mo = 2.81) revealed that the occupancy of **PMoV** in each cavity is 89.9% and 94.9%, respectively.

The  $N_2$  adsorption isotherms of 1-3 were measured at 77 K to evaluate the effects of **PMoV** encapsulation into the large cages of the *rho-*ZIF (Figure 2). The Brunauer–Emmett–



**Figure 2.**  $N_2$  adsorption—desorption isotherms of pristine *rho-ZIF*, 1, 2, and 3.

Teller (BET) surface areas of pristine *rho-ZIF*, **1**, **2**, and **3** are 1113, 379, 269, and 318 m<sup>2</sup> g<sup>-1</sup>, respectively, which suggest obvious reduction after introducing **PMoV** into the reaction systems. These results indicated that the cages in *rho-ZIF* are indeed occupied by **PMoV**.

Catalytic Oxidation. By virtue of the excellent stability in common solvents and highly ordered porosity, PMoVCrho-ZIF 1-3 are extraordinarily attractive candidates as heterogeneous catalysts. As we know, vanadium-substituted Keggin-type  $PMo_{12-n}V_nO_{40}$  (n = 1-3, PMoV) have been investigated for effectively catalyzing oxidation reactions; 19 thus, sulfether oxidation with hydrogen peroxide was selected as the model reaction for PMoVCrho-ZIF catalysts. In comparison with the homogeneous PMoV, the catalytic selectivity for sulfoxides of all PMoVCrho-ZIF systems for oxidizing thioanisoles were significantly enhanced from 51%-85% to 93%-96% (Table 1). Besides, controlled experiments were also performed for pristine rho-ZIF and a blank under the same conditions, and only ~22%-23% of thioanisoles were oxidized, which suggested that PMoV played a key role in the catalytic performance of **PMoV**⊂*rho*-ZIF.

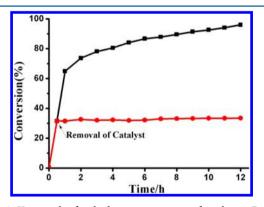
Table 1. Performance of Various Catalysts

$$\frac{H_2O_2}{\text{catalyst}} + \frac{O}{S}$$

catalyst <sup>a</sup>	conversion (%)	select for sulfoxides (%)	system
H <sub>4</sub> PMo <sub>11</sub> VO <sub>40</sub>	97	85	homo
$H_5PMo_{10}V_2O_{40}$	97	59	homo
$H_6PMo_9V_3O_{40}$	96	51	homo
$H_4$ PMo <sub>11</sub> VO <sub>40</sub> $\subset rho$ -ZIF (1)	97	96	hetero
$\begin{array}{c} \text{H}_5\text{PMo}_{10}\text{V}_2\text{O}_{40}{\subset}\textit{rho-ZIF} \\ \textbf{(2)} \end{array}$	98	97	hetero
$H_6PMo_9V_3O_{40}\subset rho$ -ZIF (3)	98	93	hetero
blank	22	95	
rho-ZIF	22	96	hetero

 $^a$ Reaction conditions: 0.25 mmol thioanisole, 0.000 45 mmol catalysis, 0.3 mmol  $\rm H_2O_2$ , 25 °C, 2 mL of methanol.

To investigate the heterogeneity of PMoVcrho-ZIF catalysts, the reaction activity of the supernatant solution after filtration of the catalyst was studied when the reaction was performed for 30 min. The reaction does not proceed after the removal of 1, implying no leaching of PMoV in the reaction process (Figure 3). More importantly, ICP-AES analysis of the filtrate



**Figure 3.** Kinetic plot for the heterogeneity test of catalyst 1. Reaction conditions: 0.25 mmol of thioanisole; 1.2 mmol of  $H_2O_2$ ; 0.000 45 mmol of 1; 2 mL of MeOH; 25 °C. The catalyst was removed from the reaction mixture after 30 min.

demonstrated that there are only traces of Mo (16 ppm), and no other metals were detected in the supernatant solution. Consistent with ICP-AES results, the UV—vis spectroscopy further confirmed that no **PMoV** were existing in the filtrate (Figure S6).

Because of the exceptional catalytic activity in the oxidation of thioanisoles, 1 was chosen as the model catalyst to optimize the reaction conditions, and the selected examples are summarized in Table 2. Several reaction variables such as the solvent, oxidant amount, reaction time, and catalyst amount were modulated to afford optimized conditions, which representatively involved 0.25 mmol of thioanisole, 0.3 mmol of  $\rm H_2O_2$ , 0.00045 mmol of catalyst, and 2 mL of methanol at 25 °C for 12 h.

To evaluate the recyclability of catalyst  ${\bf 1}$ , the catalyst was isolated by sedimentation after each experiment and then washed with EtOH and  ${\bf H}_2{\bf O}$  and dried under vacuum for using

Table 2. Effect of Reaction Conditions<sup>a</sup> for the Oxidation of Thioanisole with  $H_2O_2$ 

entry	solvent	oxygenant (mmol)	time (h)	conversion (%)	select for sulfoxides (%)
1	MeCN	0.55	18	99	4
2	EtOH	0.55	18	99	73
3	BDO	0.55	18	99	19
4	CHCl <sub>3</sub>	0.55	18	99	42
5	MeOH	0.55	18	99	79
6	MeCN	0.55	18	>99	<1
7	MeCN	0.3	18	90	70
8	MeOH	0.3	18	>99	>99
9	MeOH	0.3	8	88	>99
10	MeOH	0.3	12	99	>99

 $<sup>^</sup>aReaction$  conditions: 0.25 mmol of thioanisole, 0.00045 mmol of catalysis,  $\rm H_2O_2$  (30%), 25  $^\circ C$ , 2 mL of solvent. BDO is 1,4-butylene glycol.

in the subsequent run. As shown by Figure 4, the catalyst can be reusable with no evident loss of activity in oxidation for at

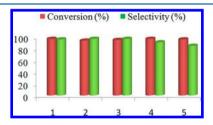


Figure 4. Recyclability of catalyst in the selective oxidation of thioanisole.

least four times, and FT-IR spectra and powder XRD of catalysts showed no obvious alteration after five cycles (Figures S7 and S8). The excellent activity and selectivity for the transformation of thioanisoles to sulfoxides of the catalyst encouraged us to explore the selective oxidation of other sulfether compounds. With optimized conditions in hand, we explored the scope of substrates with a series of valuable sulfether compounds. As shown in Table 3, it is reasonable to conclude that as the size of the substrates increase, the conversion and selectivity of substrates decrease slightly owing to the larger steric hindrance. However, the activity and selective oxidation of various sulfides retained high catalytic level.

#### CONCLUSION

In summary, one-pot mechanochemical synthesis has been demonstrated to be an efficient and environmentally friendly method to prepare host-guest POMCMOF complexes with high crystallinity, and vanadium-substituted Keggin-type POMs can be accommodated within the cavities of *rho*-type ZIF with high loading efficiency and chemical stability by physical imprisonment and cannot be released without destroying the host matrice. To our knowledge, this is the first example that metastable rho-ZIF with large interior cavities and windows is used as host matrice for encapsulating and immobilizing bulky guest molecules. More importantly, the mechanochemically prepared POMCMOF materials were used as effective heterogeneous catalyst for selective oxidation of a series of sulfides to sulfoxides and can be recycled at least four times without significant loss of activity. This work provides a versatile and efficient strategy for design and synthesis of novel catalysis systems that realize excellent dispersion and immobilization of the catalytically active centers. Further

Table 3. Substrate Expansion for Catalytic Oxidation<sup>a</sup> of Thioether by 1

Entry	Substrate	Conversion (%)	Selection for sulfoxides (%)
1	S	97.0	95.5
2	S S	92.8	84.2
3	S S	90.4	89.5
4	CI	94.4	91.3
5	O <sup>s</sup> O	82.7	89.0
6	<b>√</b> °8	97.1	92.0
7	`8'	>99	91.3

<sup>&</sup>lt;sup>a</sup>Reaction conditions: 0.25 mmol of substrates, 0.000 45 mmol of catalyst, 0.3 mmol of H<sub>2</sub>O<sub>2</sub>, 25 °C, 2 mL of MeOH.

attempts to encapsulate various guest molecules for extending the functionality of MOFs are being undertaken.

#### **■ EXPERIMENTAL SECTION**

Materials and Methods. All materials used in this work were purchased from commercial sources and used without further purification. PMoV ( $PMo_{12-n}V_n$ , n = 1-3) were produced according to a procedure described in the literature. 18a Powder XRD was performed on a Bruker Focus D8 diffractometer with a Cu K\alpha X-ray radiation source ( $\lambda$  = 0.154 056 nm). FT-IR spectra were recorded from KBr pellets in the range of 4000-500 cm<sup>-1</sup> on a Nicolet 170 SXFT-IR spectrometer. Gas chromatography (GC) analyses were performed on a Shimadzu GC-2014C with a flame ionization detector (FID) equipped with an HP-5 ms capillary column in flowing N2 with a heating rate of 5 °C min<sup>-1</sup>. GC mass spectra were recorded on an Agilent 7890A-5975C at an ionization voltage of 1200 V. C, H, and N elemental analyses were conducted on a PerkinElmer 240 °C elemental analyzer, and Mo, W, and V elemental analyses were performed on an axial view ICP-AES. The one-pot mechanochemical synthesis was performed in a ball mill (QM-3C, Nanjing University Instrument Factory, China).

**PMoV** $\subset$ *rho-ZIF.* Synthetic reactions were performed in an 80 mL zirconia milling pot with 10 mm diameter zirconia balls. One millimole of ZnO, 10 mg of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, 1.5 mmol of 2-ethylimidazole (HEtIm), 1.5 mmol of 4,5-dichloroimidazole, and 0.05 mmol of corresponding **PMoV** were put into the pot with adding 200  $\mu$ L of DEF, then the mixture was ground for 2 × 30 min at 50 Hz. The collected green solids were washed with substantial deionized water and alcohol to eliminate the excess POMs and then dried under vacuum at 80 °C for 12 h.

General Procedure for Oxidation of Sulfides by  $H_2O_2$ . Sulfides (0.25 mmol), 30%  $H_2O_2$  (0.3 mmol, 33.8 mg),  $PMoV \subset rho$ -ZIF (0.00045 mmol), and 2 mL of MeOH were added to a glass tube; then the catalytic reaction proceeded on a Wattecs parallel reactor at 25 °C for 12 h. After the reaction was completed, the resulting mixture was analyzed by GC-MS and GC.

## ASSOCIATED CONTENT

## S Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acs.inorg-chem.7b02163.

X-ray powder diffraction patterns, SEM pictures, infrared and UV-vis spectra. (PDF)

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# **Author Contributions**

All authors have given approval to the final version of the manuscript.

# Notes

The authors declare no competing financial interest.

## ACKNOWLEDGMENTS

This study was supported by the National Natural Science Foundation of China (Project Nos. 21271025, 11474204, and 21202007) and the Research Foundation of Beijing Institute of Technology (No. 20151942007).

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